

Modelling of zircaloy-4 cladding degradation in nitrogen-oxygen mixtures at 850°C

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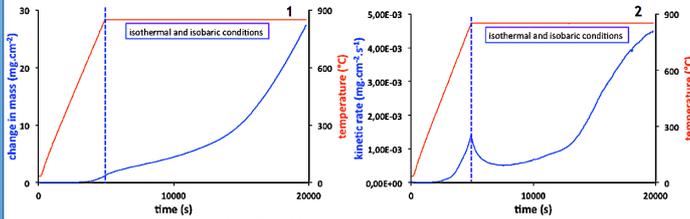


INTRODUCTION

Zy4 cladding, providing the first containment of UO₂ fuel, could be exposed to air in case of severe accident in nuclear power plant (PWR: pressurized water reactor).

Kinetic analysis is made to understand the corrosion mechanism of Zy4 plates at 850°C in nitrogen and oxygen mixtures during **post-transition stage** :

- does the corrosion proceed in a steady-state ?
- is the assumption of a rate-determining step confirmed?
- what is the influence of oxygen and nitrogen partial pressures on the kinetic rate and how could it be explained?



Thermogravimetric test at 850°C in 20% O₂ - 80%N₂ mixture; 1 change in mass as a function of time and 2 derivation versus time of the change in mass (kinetic rate)

EXPERIMENTS

Thermogravimetric tests

Symmetrical balance Setaram TAG-24

Plates of recrystallized Zy4 (10mm x 10mm) : 1.32-1.35 wt.% Sn

Experimental conditions :

- O₂ - N₂ - He or Ar flowing mixtures (10 L.h⁻¹)
- heat-up ramp to 850°C : 10°C.min⁻¹
- total pressure: 1 atm

KINETICS TESTS

Steady-state and rate-determining step assumptions validation⁽¹⁾:

$$\frac{d\left(\frac{\Delta m}{S}\right)}{dt} = \frac{n_0 \cdot M(O_2)}{S} \cdot \frac{d\alpha}{dt} = \frac{n_0 \cdot M(O_2)}{S} \cdot \Phi \cdot Sm(t)$$

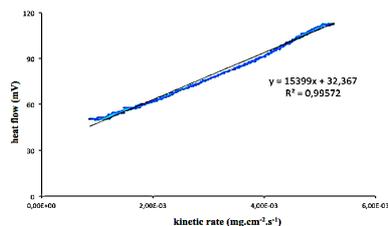
1) Steady-state approximation:

Heat flow (dQ/dt) versus mass gain rate (dΔm/dt)

→ test validated if the kinetic rates measured by the two methods are proportional

$$\frac{d\Delta m}{dt} = - \frac{\sum G_i(M_{G_i} \cdot v_{G_i})}{\Delta H} \cdot \frac{dQ}{dt}$$

- ΔH: enthalpy of reaction
 - M_{G_i}: molar mass of gas
 - n_{G_i}: stoichiometric number of gas



Steady-state test in 20% O₂ - 80%N₂ mixture

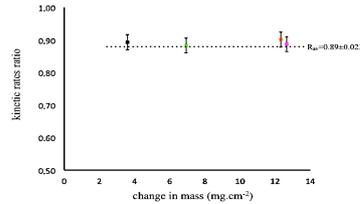
2) Rate-limiting step assumption: ΦSm test jumps method

Jumps from temperature T₁ to temperature T₂ for experiments conducted up to various change in mass (t_a, t_b, etc.)

→ determination of the ratio of kinetic rates after and before the jump

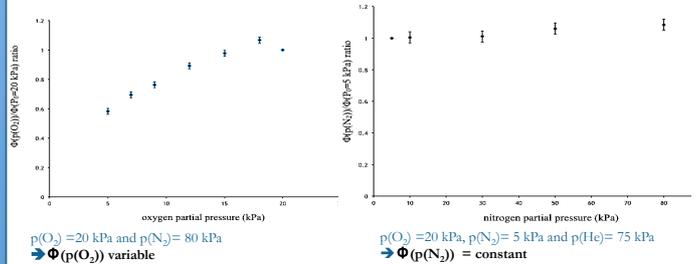
$$R = \frac{\left(\frac{d\left(\frac{\Delta m}{S}\right)}{dt}\right)_2}{\left(\frac{d\left(\frac{\Delta m}{S}\right)}{dt}\right)_1} = \frac{B_0 \cdot \Phi(T=830) \cdot Sm(t_a)}{B_0 \cdot \Phi(T=850) \cdot Sm(t_b)} \cdot \frac{B_0 \cdot \Phi(T=830) \cdot Sm(t_b)}{B_0 \cdot \Phi(T=850) \cdot Sm(t_a)} = \frac{\Phi(T=830)}{\Phi(T=850)}$$

ΦSm test in 20% O₂- 80%N₂ mixture with temperature jumps from 850°C to 830°C. Kinetic rates ratio obtained for various change in mass is constant:
R = 0.89 → a rate determining step controls the growth process



3) Pressure jumps : study of Φ(p(O₂)) and Φ(p(N₂))

Pressure jumps at 8mg.cm⁻² : p(N₂) or p(O₂) changes



p(O₂) = 20 kPa and p(N₂) = 80 kPa
→ Φ(p(O₂)) variable

p(O₂) = 20 kPa, p(N₂) = 5 kPa and p(He) = 75 kPa
→ Φ(p(N₂)) = constant

4) Zy-4 post-transition sample



"Porosity" of the oxide layer due to:
→ cracks during ZrN creation
→ cracks in dense zirconia during oxidation of ZrN

MODELLING - CONCLUSION

Optical micrography + SEM → 3 reactions



PBR_{ZrO₂/ZrN} = 1,47



PBR_{ZrN/Zr} = 1,03

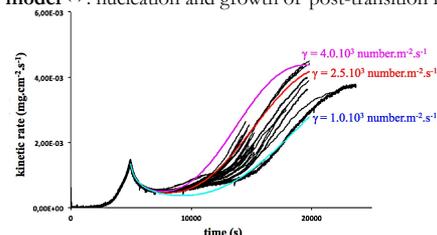


PBR_{ZrO₂/Zr} = 1,51

Steady-state and rate-determining step assumptions have been validated.

-Φ modelling: kinetic rate strongly dependant of p(O₂)
→ controlled by interfacial reaction step of ZrN oxidation

-Sm modelling: non uniform appearance of post-transition regions → nucleation
→ Mampel's model⁽²⁾: nucleation and growth of post-transition regions



Comparison of the model with experimental results
Conditions : flow rate = 10 L/h, p(O₂) = 20 kPa, p(N₂) = 80 kPa, T = 850°C

References

- (1) M. Pijolat & al., *Thermochim. Acta* 478, 34 (2008)
- (2) B. Delmon, "Introduction à la cinétique hétérogène", Technip Editions, Paris (1969)